



Optimization and Modeling of Microcystin-LR Degradation by TiO₂ Photocatalyst Using Response Surface Methodology

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ABSTRACT

Introduction: Microcystin-leucine arginine (MC-LR) is a toxin with harmful effects on the liver, kidney, heart, and gastrointestinal tract. So, effective removal of MC-LR from water resources is of great importance. The aim of this study was to remove microcystin-LR (MC-LR) from aqueous solution by Titanium Dioxide (TiO₂).

Materials and Methods: In the present study, TiO₂, as a semiconductor, was used for photodegradation of MC-LR under ultraviolet light (UV). The Response Surface Methodology was applied to investigate the effects of operating variables such as pH (A), contact time (B), and catalyst dose (B) on the removal of MC-LR. The MC-LR concentration was measured by high-performance liquid chromatography (HPLC).

Results: The results showed that single variables such as A, B, and C had significant effects on MC-LR removal ($p_{\text{value}} < 0.05$). In other words, increase of the contact time and catalyst dose had a positive effect on enhancing the removal efficiency of MC-LR, but the effect of pH was negative. The analysis of variance showed that BC, A², and C² variables had a significant effect on the MC-LR removal ($p_{\text{value}} < 0.05$). Finally, the maximum removal efficiency of MC-LR was 95.1%, which occurred at pH = 5, contact time = 30 minutes, and catalyst dose = 1 g/l.

Conclusion: According to the findings, TiO₂, as a photocatalyst, had an appropriate effect on degradation of the MC-LR.

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Introduction

Algal blooms and cyanobacteria species can cause many problems for drinking water resources by generating cyanotoxins^{1, 2}. Presence of cyanobacterial, as biological pollution, in freshwater environments has adverse effects on the water quality including its taste, odor, color, and even microbial diversity^{3, 4}. Discharge of nutrients, such as Nitrogen and Phosphorus, from agricultural watersheds to the

freshwater resources is a major cause of cyanobacterial propagation^{5, 6}. Popular algal bloom-forming species include *Aphanizomenon*, *Cylindrospermopsis*, *Dolichospermum*, *Microcystis*, *Nodularia*, and *Planktothrix* and *Trichodesmium*⁷. Toxins of cyanobacteria include hepatotoxins, neurotoxins, cytotoxins, dermatotoxins, and gastrointestinal toxins that threaten the human and the environment health⁸⁻¹¹. Among 80 variants of the cyanotoxin family, microcystins (MCs) are the

most well-known^{12, 13}. Furthermore, microcystin-LR (MC-LR) is one of the most toxic members of the microcystins group^{10, 14}. Microcystin-LR is hepatotoxic; acute and chronic exposure to MC-LR can lead to liver cancer in humans and have harmful effects on the kidney, heart, and gastrointestinal tract¹⁵⁻¹⁷. The World Health Organization (WHO) recommended the permissible level of 1 µg/L of MC-LR in the drinking water^{18, 19}. So, the removal of MC-LR from drinking water resources is very necessary for human health and environmental safety¹⁰. Many treatment methods, such as coagulation, flocculation, activated carbon adsorption, rapid sand filtration, and membrane separation were used for removing MC-LR from water body^{14, 18, 20}. In this regard, the traditional water treatment systems can remove cyanobacterial cells, but they have limited capability in removing cyanotoxins due to different practical, economic, or environmental disadvantages^{21, 22}. The traditional treatment process can also release cyanotoxins into the water by ripping the cyanobacterial cells, which increases the risk of secondary pollution²³. In the past decade, the Advanced Oxidation Process (AOPs), such as photocatalytic oxidation process, have received significant attention due to their effectiveness in degradation and mineralization of the resistant compounds such as cyanotoxins^{24, 25}. Various studies used the photocatalytic oxidation process to remove the environmental pollutants. For example, ZnO, UV-H₂O₂ and bismuth vanadate (BiVO₄) is used for removal of microcystin-LR, Cyanobacterial taste and bisphenol A, respectively^{6, 26-28}. The effect of TiO₂ was studied for degrading various pollutants, such as Azo dye, phenol, humic acid, nodularin, and cyanotoxin. The results showed that TiO₂ had high efficiency in the removal of these pollutants²⁹⁻³². The photocatalytic oxidation process is a green

technology that mineralizes the organic molecules into CO₂ and inorganic ions by producing strong reactive oxidizing species like hydroxyl radicals (OH[•]), superoxide anion radical (O₂^{•-}), and hydroperoxyl radical (HO₂[•])^{18, 37, 38}. Among the photocatalytic oxidation technologies (POTs), Titanium dioxide (TiO₂) is a highly effective semiconductor material able to decompose water contaminations effectively; TiO₂ has favorable properties such as high chemical and thermal stabilities, nontoxicity, commercial availability, and low cost³⁵. Usually, TiO₂ can generate photo-excited electron-hole pairs by absorbing ultraviolet light. Later, the photo-excited electron-hole pairs reduce and oxidize the reactants adsorbed on the semiconductor surface. So, the reduction and oxidation reactions are the major mechanisms in water photocatalytic purification^{32, 33}. So, the aim of this study was to find the optimum condition for the TiO₂ photocatalyst in removing MC-LR under UV light using Response Surface Methodology (RSM) based on the Central Composite Design (CCD).

Materials and methods

Materials

Microcystin-LR (MC-LR) (Molecular Formula: C₄₉H₇₄N₁₀O₁₂, Molecular Weight: 995.2 g/mol) was considered as the standard solution (10 µg/ml) purchased from Sigma-Aldrich (Figure 1). Furthermore, TiO₂ nanopowder (≥ 99% anatase) was prepared from Sigma-Aldrich Co. (USA). The standard solutions were prepared by dissolving standard powder of MC-LR in 1 ml of methanol (100%) and diluted with distilled water (Merck co, Germany). All solutions were stored at 4 °C until use¹⁴. The other chemical materials such as methanol, acetonitrile, trifluoroacetic acid (TFA) (HPLC-grade), sodium hydroxide, and Hydrochloric acid were purchased from Merck Company (Germany).

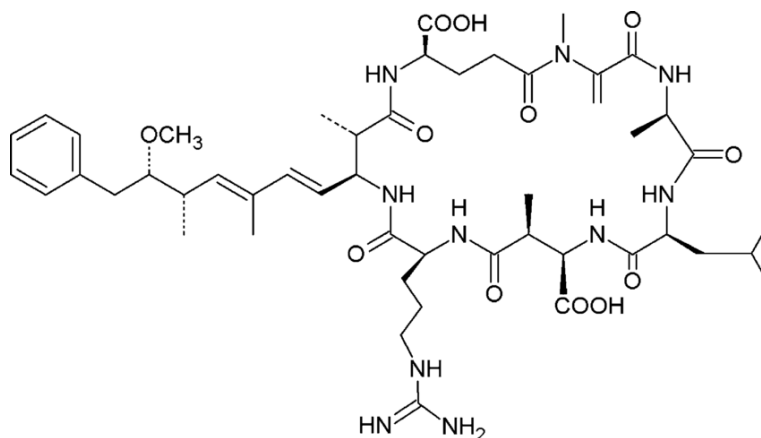


Figure 1: The molecular structure of MC-LR

All experiments were conducted with a mixture of catalysts; 10 ml of aquatic solutions were mixed with 500 µg/L MC-LR in 25 ml Pyrex beakers. For adjusting the pH of samples, NaOH (0.01M) and (0.01M) HCl were used. The aggregates were eliminated and then the samples were located in an ultrasonic bath (10 min). For photocatalyst suspensions, 100 W mercury lamp (wavelength of 254 nm) was placed 10 cm above the Pyrex beakers. Initially, the samples were stirred (30 min) in darkness to reach the balance. In addition, UV lamps were turned on and placed under magnetic stirring to keep the suspension uniformity. At the end of the required contact time, UV lamps were turned off and samples were taken. Before measuring the residual MC-LR content by HPLC, the samples were filtrated with syringe filters (0.22 µm) to separate the catalyst particles.

Characterization study

To investigate the structure and surface morphology of TiO₂ nanoparticles, the field emission scanning electron microscope (FESEM) (FEI Quanta 200, USA) and X-ray diffractometer (XRD, Bruker D8 Advance, Germany) were used. Moreover, the FTIR spectrum of TiO₂ was studied by an IR spectrometer (Jasco 6300, Japan).

Design of experiments

In this study, RSM was used to optimize the number of experiments and to evaluate the interactive effects of the significant operating parameters in the MC-LR degradation by TiO₂ photocatalysts using the Design-Expert software 10³⁸⁻⁴¹. According to the Central Composite Design (CCD), as the most widely used method in evaluating interactive effects of the operating parameters, three variables of pH (A), contact time (B), and catalyst dose (C) were selected as the model variables (Table 1).

Table 1: Actual and coded values of the independent variables using CCD

| Variables | Unit | Actual values of the coded values | | | | |
|-------------------|------|-----------------------------------|-----|-----|----|-----|
| | | -2 | -1 | 0 | +1 | +2 |
| pH (A) | | 4 | 5 | 7 | 9 | 10 |
| Contact time (B) | min | 5 | 10 | 20 | 30 | 35 |
| Catalyst dose (C) | g/l | 0.2 | 0.4 | 0.7 | 1 | 1.2 |

The coded values of independent variables were determined using Eq. (1):

$$Xi = \frac{(Xi - X0)}{\Delta X} \tag{1}$$

Where, Xi is a coded value of the independent variable, X₀ is the center point value, and ΔX is the

change value⁴⁰. To study the interaction among the independent and dependent variables, the regression model was used (Eq. (2)):

$$Y = \beta_0 + \sum \beta_i X_i + \sum \beta_{ii} X_i^2 + \sum \beta_{ij} X_i X_j \tag{2}$$

Where, Y is the predicted response of the MC-LR removal, β_0 is the model constant, β_i is the linear coefficient, β_{ii} is the quadratic coefficient, and the β_{ij} is the cross product coefficient.

Analysis and calculation

The concentration of MC-LR was quantified using an HPLC system (Jasco PU-2080, Tokyo, Japan) equipped with a quaternary mixing pump, an inline vacuum degasser, UV-Vis detector (UV-2075 plus), and an auto-injector (AS-2055 Plus). Samples were separated by the C₁₈ column (150 × 4.6 mm, 5 μm particles). Combination of acetonitrile and Milli-Q water with a volume ratio of 50:50 plus 0.1% fluoroorotic acid (TFA) was used as the mobile phase with a flow rate of 1 ml/min. Due to the typical absorption spectra of

MC-LR, the wavelength of UV detector was set at 238 nm⁴². The injection volume was 100 μl with a flow rate of 1 ml/min and the total run time was 15 min. The Borwin Chromatography software (Version 1.50) was used for data acquisition and HPLC processing. MC-LR degradation rate was determined by (Eq. (3)):

$$\text{Degradation rate (\%)} = C_0 - C/C_0 * 100 \quad (3)$$

Where, C_0 and C are the initial and the residual concentrations of MC-LR, respectively.

For validating the analytical method, the relative recovery, limit of detection (LOD), and limit of quantification (LOQ) were calculated according to the recommendations set by the International Conference on Harmonization (ICH) (Table 2).

Table 2: Analytical method validation parameters for determination of MC-LR by HPLC

| Parameter | Recovery (%) | LOD (μg/L) | LOQ (μg/L) |
|-----------|--------------|------------|------------|
| MC-LR | 102 ± 9.5 | 4.04 | 12.24 |

Ethical issues

This study was conducted with approval of Isfahan University of Medical Sciences. Research Ethics Code was IR.MUI.REC.1395.3.847.

Results

Characterization study

The TiO₂ photocatalysts was characterized by FESEM, FTIR, and XRD (Figure 2). These TiO₂ particles have asymmetrical and angular shapes (Figure 2a). Figure 2b shows the FTIR spectra of TiO₂ nanoparticles. In the FTIR spectra of TiO₂,

the wavelength of 3408 cm⁻¹ was associated with the Hydroxide bonds (O-H), indicating the presence of water and moisture molecules. Furthermore, the wavenumber 455 cm⁻¹ was related to the metal hydroxides bonds^{40, 41}. The spectrum of XRD related to the TiO₂ is demonstrated in Figure 2c. According to the XRD patterns, the index peaks of synthetic TiO₂ located at about $2\theta = 25.33^\circ, 37.8^\circ, 30.57^\circ, 48.1^\circ,$ and 53.9° correspond well to the anatase phase of TiO₂⁴³⁻⁴⁵.

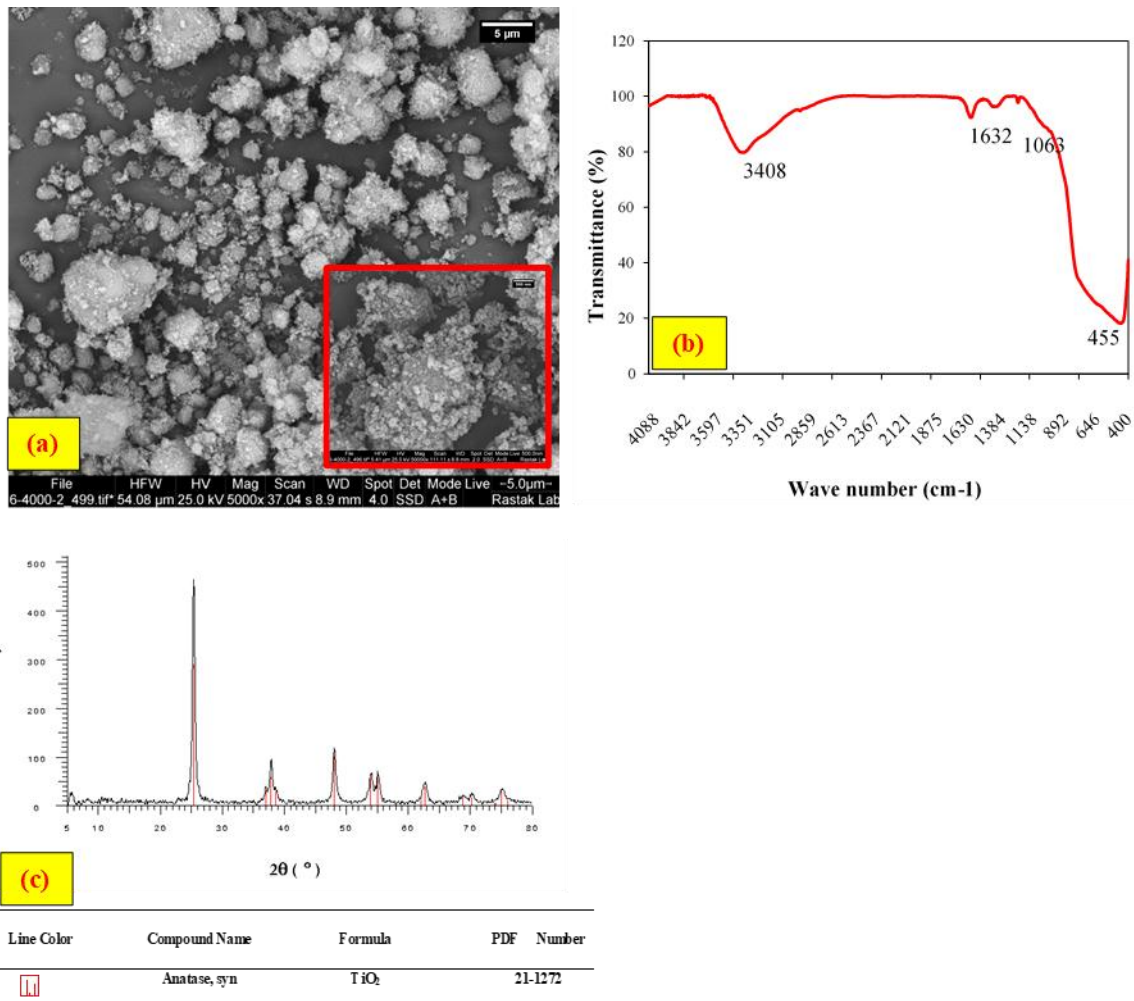


Figure 2: SEM (a), FTIR (b), and XRD (c) graphs of TiO₂ catalyst

Analysis of variance and model fitting

Eventually, 20 different experimental runs were designed by CCD, which are portrayed in Table 3 along with the predicted and actual MC-LR removal values. The results of analysis of variance for the removal of MC-LR are presented in Table 4. According to this table, F-value of the quadratic model was 80.78, indicating that the model was significant. If the “Prob > F” value of each parameter was less than 0.05, the effect of this parameter effect on MC-LR removal is significant. Therefore, single parameters of A, B, and C are significantly different. Except for AB, AC, and B², the P-values related to the interactions of BC, A², and C² were less than 0.05 and indicated a significant effect on the MC-LR

removal (p-value = 0.0410, 0.0001, and P = 0.0382, respectively). So, other quadratic forms did not have any significant effect on the model and could be removed from the final equation. The F-value lack of fit in this model was 3.23, showing that the lack of fit was not significant. In other words, the model fitted (p-value > 0.05) the experimental data and errors of the experiments were low. The values of R² and adj R² were 0.9864 and 0.9742, respectively, demonstrating that the results of the model were fitted to the experimental results. Finally, these relations showed that this model was significant. To investigate the effects of variables, all experiments were carried out in various combinations of the variables; they were

statistically designed using central composite design (CCD). To access a final model with significant predictors, insignificant (p-value > 0.05) interactions were eliminated from this model. Thus, other significant variables were retained in the final regression model. So, the

following equation was derived as the final equation using coefficient of the coded variables for removal of MC-LR (Eq. 4):

$$\text{Removal of MC-LR (\%)} = 76.05 - 5.44 A + 3.94 B + 7.48 C - 1.16 BC + 3.38 A^2 + 1.02 C^2 \quad (4)$$

Table 3: Experimental design conditions and responses of various experimental run

| Run. no | Variables | | | MC-LR removal (%) | |
|---------|-----------|-----------------------|------------------------|-------------------|-----------|
| | A: pH | B: Contact time (min) | C: Catalyst dose (g/l) | Actual | Predicted |
| 1 | 5 | 10 | 1 | 90.70 | 89.42 |
| 2 | 9 | 10 | 1 | 78.60 | 79.99 |
| 3 | 9 | 30 | 1 | 85.10 | 85.03 |
| 4 | 5 | 10 | 0.4 | 73.40 | 73.05 |
| 5 | 5 | 30 | 1 | 95.10 | 95.50 |
| 6 | 7 | 20 | 0.7 | 75.42 | 76.05 |
| 7 | 7 | 20 | 0.7 | 77.35 | 76.05 |
| 8 | 7 | 20 | 0.7 | 76.37 | 76.05 |
| 9 | 7 | 20 | 0.24 | 65.80 | 67.00 |
| 10 | 7 | 35.25 | 0.7 | 80.80 | 81.02 |
| 11 | 5 | 30 | 0.4 | 85.60 | 83.79 |
| 12 | 9 | 10 | 0.4 | 62.60 | 61.78 |
| 13 | 9 | 30 | 0.4 | 70.60 | 71.46 |
| 14 | 7 | 20 | 0.7 | 74.99 | 76.05 |
| 15 | 7 | 20 | 0.7 | 75.53 | 76.05 |
| 16 | 7 | 20 | 0.7 | 77.10 | 76.05 |
| 17 | 10 | 20 | 0.7 | 76.70 | 75.62 |
| 18 | 7 | 4.75 | 0.7 | 68.50 | 69.00 |
| 19 | 4 | 20 | 0.7 | 90.40 | 92.20 |
| 20 | 7 | 20 | 1.16 | 90.30 | 89.82 |

Table 4: The results of analysis of variance in removing MC-LR

| Source | Sum of Squares | df | Mean Square | F Value | p value Prob > F |
|------------------|----------------|----|-------------|---------|------------------|
| Model | 1429.02 | 9 | 158.78 | 80.78 | < 0.0001 |
| A: pH | 374.08 | 1 | 274.08 | 190.3 | < 0.0001 |
| B: Contact time | 196.48 | 1 | 196.48 | 99.96 | < 0.0001 |
| C: Catalyst dose | 708.3 | 1 | 708.3 | 360.33 | < 0.0001 |
| AB | 0.55 | 1 | 0.55 | 0.28 | 0.6068 |
| AC | 1.71 | 1 | 1.71 | 0.87 | 0.3728 |
| BC | 10.81 | 1 | 10.81 | 5.50 | 0.0410 |
| A ² | 123.75 | 1 | 123.75 | 62.96 | < 0.0001 |
| B ² | 2.14 | 1 | 2.14 | 1.09 | 0.3216 |
| C ² | 11.20 | 1 | 11.20 | 5.70 | 0.0382 |
| Residual | 19.66 | 10 | 1.97 | | |
| Lack of Fit | 15.01 | 5 | 3.00 | 3.23 | 0.1122* |
| Pure Error | 4.65 | 5 | 0.93 | | |
| Cor. Total | 1448.68 | 19 | | | |

Std. Dev.: 1.40; Mean: 78.55; C.V. %: 1.78; PRESS: 136.74; R₂ : 0.9864; Adj R₂ : 0.9742; Pred R₂ : 0.9056; Adeq. Precision: 34.08.

*not significant

The correlation between actual, predicted, and normal graphs of the residuals in removing MC-LR are presented in Figures 3a and b. According to

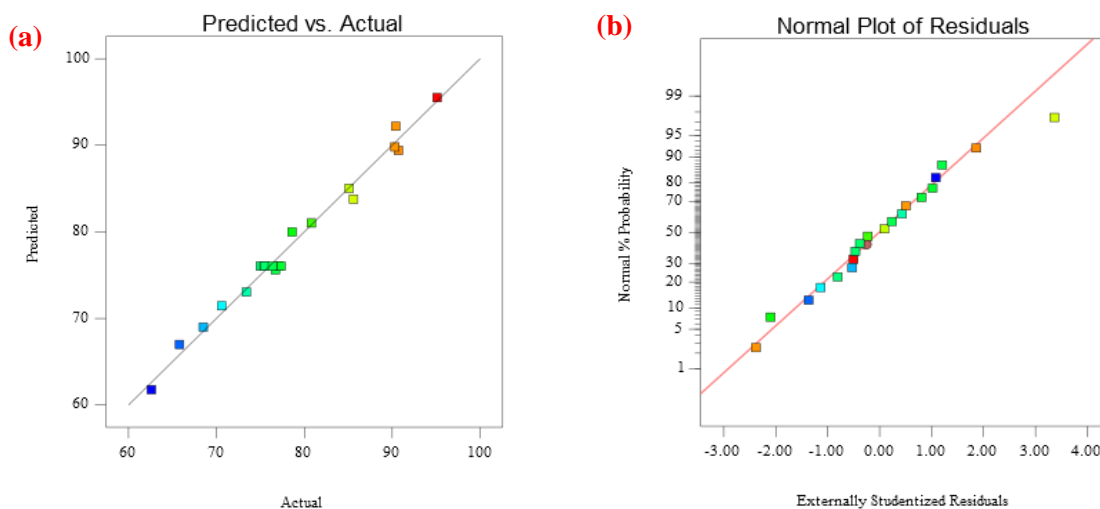


Figure 3: Model evaluation plots for the removal of MC-LR by TiO₂: the experimental data vs. the predicted value plot (a); the normalized residual plot (b)

Discussion

Effect of variables on photocatalytic degradation of MC-LR

Effect of single factors

Among the pH, contact time, and catalyst dose variables, factors with high mean square and high F-value had the highest effect on the photodegradation of MC-LR by TiO₂. So, Catalyst dose (c) with mean square = 703.3 and F-value = 360.3 were the most important parameters in MC-LR removal. Moreover, the pH and contact time variables had lower importance than catalyst dose in MC-LR degradation.

Effect of pH

The effect of pH on the removal of MC-LR at various ranges of pH is presented in Figure 4a. This figure shows that the pH variable has a negative effect on MC-LR removal. So, the degradation rate of MC-LR increased with decrease of the pH. Therefore, the results indicated that MC-LR removal had increased in the acidic range. Generally, in photocatalytic systems, the acidic range was determined considering the strong electrostatic adsorption between the positive charges of catalyst and the negative charges of toxin were

these figures, data distribution shows a straight line, which indicates that the experimental data are fitted by the response predicted values.

determined as the optimal pH in photocatalytic degradation of toxins. So, the forces between the catalyst particles and MC-LR molecules were attractive forces resulting in high photodegradation⁴². Samy et al. reported that the photocatalytic degradation of chlorpyrifos was increased in the acidic pH due to the effect of attractive forces between the catalyst particles and chlorpyrifos molecules⁴⁶. In addition, other similar studies showed that the removal efficiency of direct red 16 (DR16), methylene blue, and Acid Blue 113 dyes was decreased in alkaline pH. In acidic pH, photocatalytic activity was improved by electrostatic force interactions between dye molecules and surface of the catalyst⁴⁷⁻⁴⁹. Fakhravar et al. reported that the degradation rate of Metronidazole increased with decrease of the initial pH⁵⁰.

Effect of irradiation time

Figure 4b demonstrates the effect of contact times on the removal efficiency of MC-LR using TiO₂ photocatalysts. The results indicated a positive relationship between contact time and MC-LR degradation. In other words, increase of the contact time enhances the MC-LR removal efficiency

because increase of the contact time enhances the reaction time, and increases probability of the interaction between MC-LR and electron-hole pair subsequently. Rahimi et al. showed that degradation rate of acid orange 10 increased by increase of the contact time. In other words, when the contact time increased from the start of the process to 150 min, the removal efficiency reached from 0 to 94%⁴¹. Similar studies by Sheikh Asadi et al. and Rafiee et al. reported that enhancing the contact time increased the removal efficiency of Bisphenol A and DR16 dye, respectively. This is due to the fact that increased contact time enhanced the photocatalytic activities in the catalyst surface^{51, 52}.

Effect of catalyst dose

The effect of the TiO₂ catalyst dose on the removal efficiency of MC-LR is represented in

Figure 4c. This figure shows that the degradation rate of MC-LR increases with increasing TiO₂ catalyst dose because the active sites of catalysts rise and cause absorption of MC-LR and light, which increase the photocatalytic degradation consequently. Zhang et al. reported that degradation rate of the MC-LR enhanced with the increase of catalyst dose due to the surface area of the catalyst⁵³. Koh et al. and Arabzadeh et al. reported that the photodegradation rate of Methylene Blue (MB) and tartrazine enhanced when the catalyst dose increased, respectively. Increase of the catalyst dose can enhance the photocatalytic active sites to absorb more photons. This generates more hydroxyl and superoxide radicals and finally degrades more pollutant molecules^{54, 55}. Therefore, given the cost and effects of the catalyst, choosing the optimum catalyst dose is very indispensable.

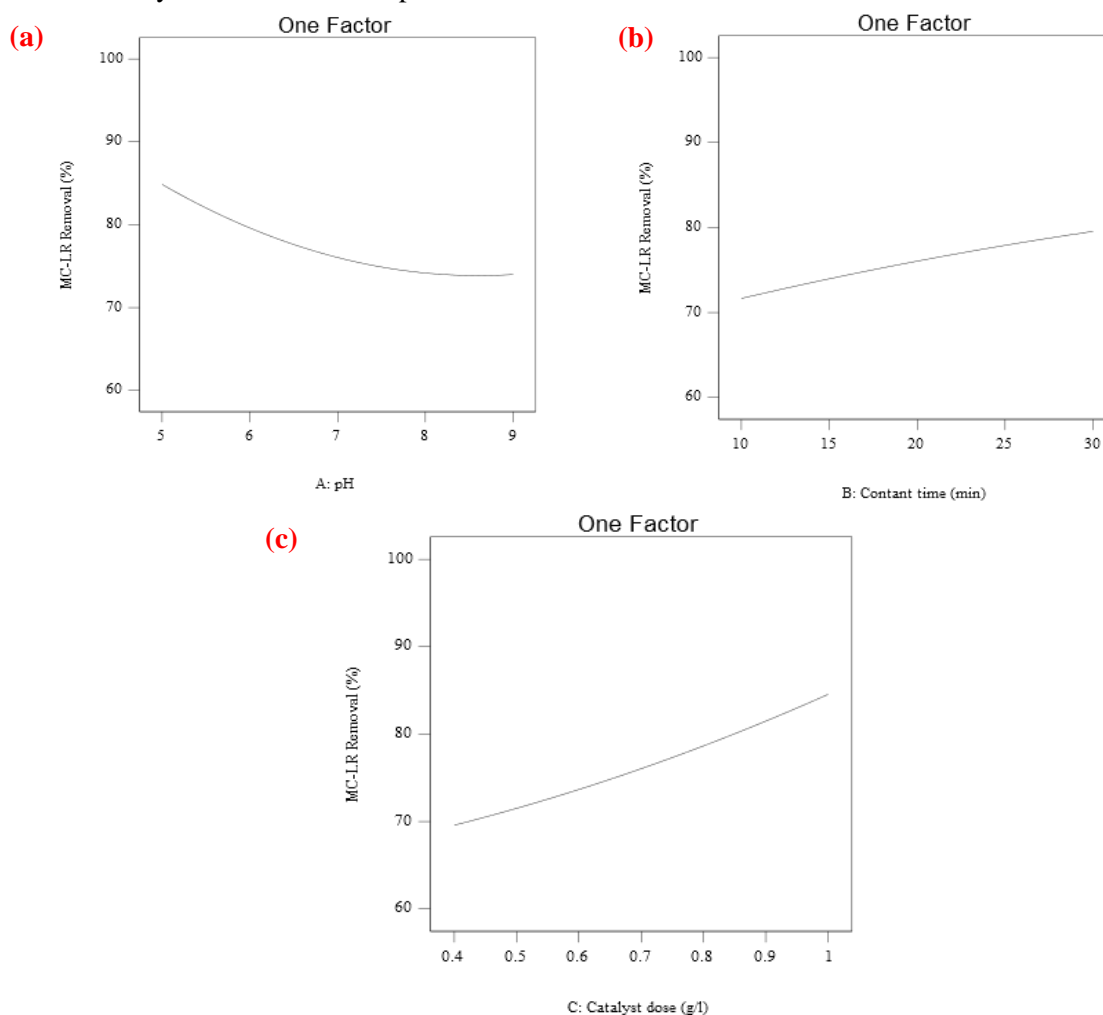


Figure 4: The effect of pH (a), contact time (b) and catalyst dose (c) on MC-LR degradation (%)

Interaction relationship between studied variables

Figure 5 illustrates the effects of interactions between different variables in the MC-LR degradation (%) by the 3D-dimensional surface-response plots gained from the quadratic model. Figure 5a shows the 3-D response surface plot of the MC-LR removal efficiency in various contact times vs. pH. According to this figure, a decrease in pH and an increase in contact time, increased the removal efficiency of MC-LR. The effect of the pH on MC-LR degradation in this figure is more evident than the contact time. However, ANOVA results showed that P-value of the interaction effect coefficients of the contact time and pH was equal to 0.6068, which is not significant. The interaction effect between

catalyst dose and pH in the MC-LR degradation (%) is illustrated in Figure 5b. As it shows, increase of the catalyst dose and reduction of the pH boost the MC-LR removal efficiency. However, the ANOVA results indicated that interaction effect coefficients of the catalyst dose and pH were not significant (P-value = 0.3728) and did not display any interaction effects. Figure 5c shows that the catalyst dose and contact time had a positive effect on the removal efficiency of MC-LR. This means that the catalyst dose and contact time display interaction effects on MC-LR removal. Moreover, the ANOVA results approved that interaction effect coefficients of these two parameters were significant (P-value = 0.0410).

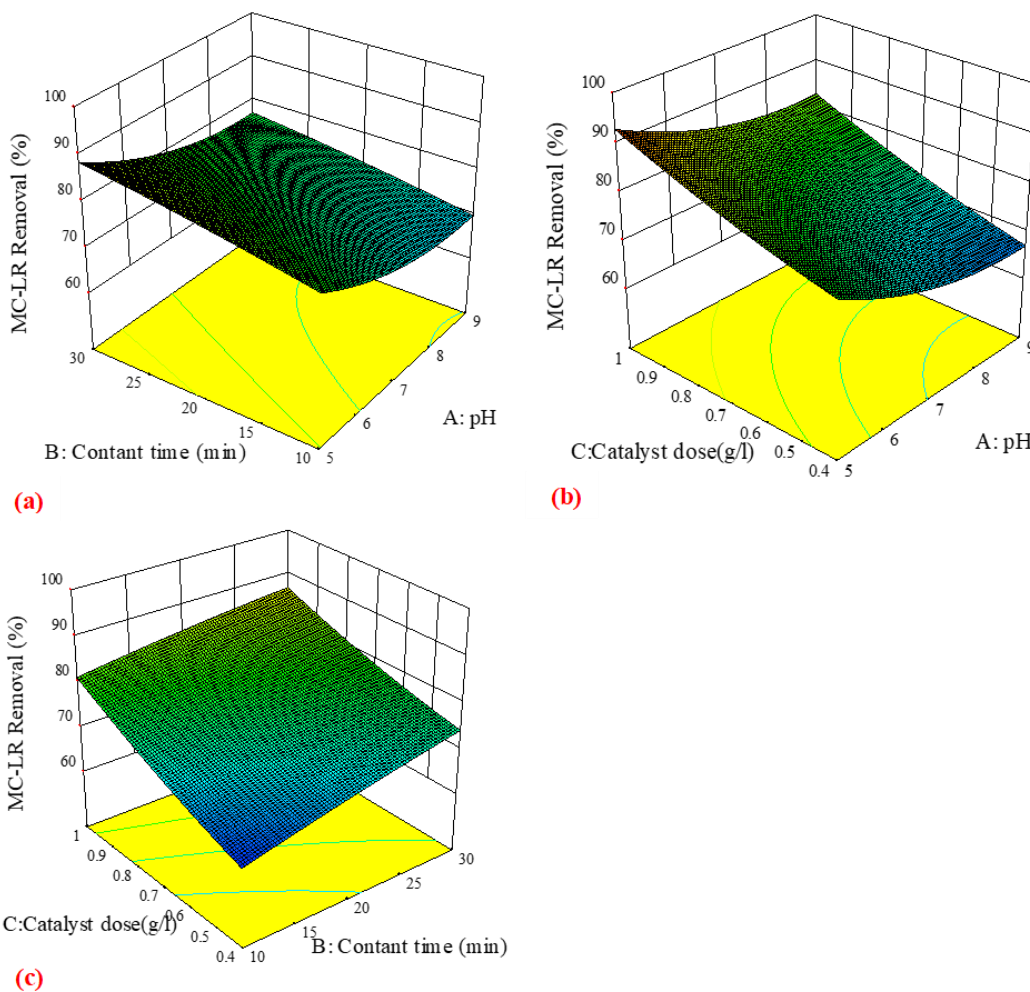


Figure 5: Interaction between different variables: (a) Contact time vs. pH; (b) Catalyst dose vs. pH; (c) Catalyst dose vs. Contact time in the MC-LR degradation (%)

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Optimization of various process parameters

The optimum amount of various variables including pH (A), contact time (B), and catalyst dose (C) in the removal of MC-LR were optimized by the RSM model. The desirable goal in the RSM model was set on the maximum removal percentage of MC-LR. So, the highest MC-LR removal efficiency was about 95.1% at these conditions: pH = 5, contact time = 30 min and catalyst dose = 1 g/l. Finally, in order to estimate the validity of optimal conditions in the removal of MC-LR, a series of experiments were performed. The findings showed a good accordance between these results and predictions of Design Expert.

Photocatalytic mechanism

TiO₂ absorbed photons, was excited, and generated e⁻ and h⁺ pairs⁵⁶. The photodegradation reactions are occurring in the presence of ultraviolet (UV) light source. Initially, a photon is absorbed by the photocatalyst after irradiating the

UV light. This causes charge separation and excites an e⁻ to the conduction band (CB) of the catalyst. As a result, [•]OH is generated by oxidation of H₂O molecules with photogenerated holes and oxygenated species that attack the MC-LR molecules. The generated e⁻ by photon absorption, either react with oxygen absorbed on the catalyst surface or react with H₂O to produce [•]O₂⁻ radicals or it may reduce the MC-LR (Figure 6). The hole (h⁺) is responsible for generating [•]OH radicals by reacting with OH ions or H₂O^{35, 57, 58}. When [•]OH radical is formed, it reacts instantly⁵⁹. The probable photochemical reactions in the degradation of MC-LR by TiO₂ are presented as follows:

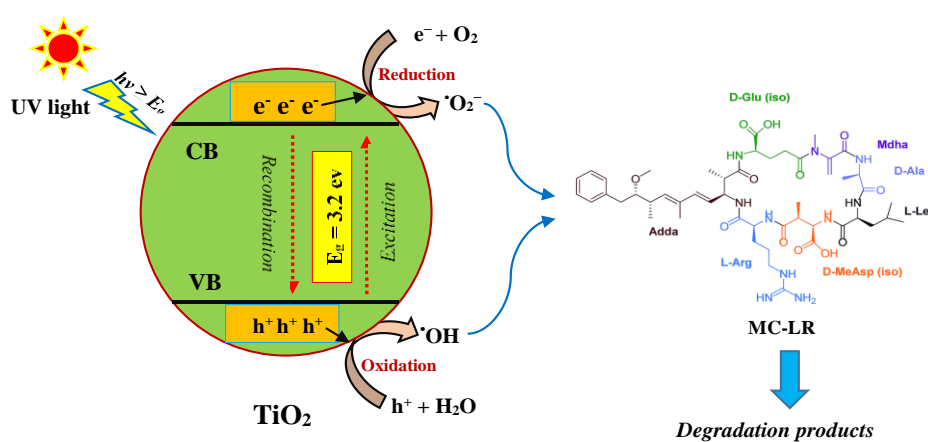
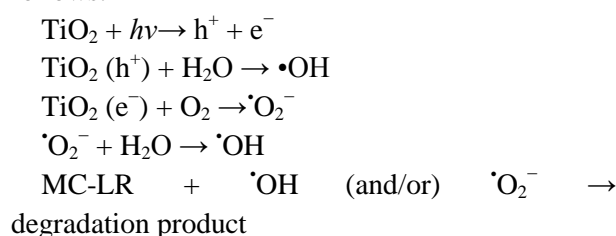


Figure 6: Degradation mechanism of MC-LR.

1072 Conclusions

The results showed that increased contact time and catalyst dose as well as reduction of pH boosted the removal efficiency of MC-LR. According to the results, the highest removal efficiency of MC-LR was 95.1% that was observed in pH = 5, contact time = 30 min, and catalyst dose = 1 g/l. According to the findings, TiO₂, as a common photocatalyst had a suitable effect on

degradation of MC-LR. However, we suggest combining TiO₂ with metal and non-metallic semiconductors to increase the removal efficiency of MC-LR. Moreover, it can be concluded that RSM is one of the efficient methods for decreasing costs and the number of experiments.

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Conflict of interest

Authors declare no conflict of interest.

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