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ORIGINAL RESEARCH PAPER

Photodegradation process for the removal of acid orange 10 using titanium dioxide and bismuth vanadate from aqueous solution

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ABSTRACT

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In this study, the photocatalytic degradation of azo-dye acid orange 10 was investigated using titanium dioxide catalyst suspension, irradiation with ultraviolet-C lamp and bismuth vanadate under visible light of light-emitting diode lamp. Response surface methodology was successfully employed to optimize the treatment of acid orange 10 dye and assess the interactive terms of four factors. The characteristics of catalysts were determined by field emission scanning electron microscopes, X-ray diffraction and Fourier transform infrared spectroscopy. The optimum values of initial dye concentration, initial pH, irradiation time and catalyst dose were found 11.889 mg/L, 4.592, 12.87 min, and 0.178 g/100 mL for ultraviolet/titanium dioxide process, respectively, and 10.919 mg/L, 3.231, 320.26 min and 0.239 g/100 mL for visible/bismuth vanadate process, respectively. The removal efficiencies obtained for acid orange 10 were 100% and 36.93% after selecting the optimized operational parameters achieved for titanium dioxide and bismuth vanadate, respectively. The highest

efficiency was achieved by the use of ultraviolet/titanium dioxide system, while a low acid orange 10 removal efficiency was obtained for the synthesized bismuth vanadate using the co-precipitation method. Thus, it seems necessary to increase the photocatalytic activity of bismuth vanadate in combination with titanium dioxide to remove acid orange 10 dye in subsequent studies.

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INTRODUCTION

By discharging substantial amounts of pollutants into the natural environment, serious soil and water pollution are produced daily (Nong *et al.*, 2011).

Several studies have reported that azo dyes are an important category of water soluble artificial colors widely used in textile industry, accounting for 1% to 50% of all commercial dyes (Aleboyeh *et al.*, 2008; Armağan *et al.*, 2003; Saien and Soleymani, 2007). The removal of these pollutants is an important challenge for the environmental engineers. There are aromatic rings in the molecular structures of azo dyes, which make the wastewaters poisonous

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and largely indestructible as a significant source of environmental pollution (Carmen and Daniela, 2012). A small amount of dyes (below 1 mg/L) has a significant impact on the quality of water (Rafatullah et al., 2010). Discharge of such colored effluents into the environment is known as a significant source of pollution causing chemical reactions to occur in the wastewater phase (Udom et al., 2013). In general, the effective methods for the treatment of dyecontaining sewage can be classified into two types: 1) decoloration by physical and chemical methods, and 2) biodegradation. The traditional physical methods such as activated carbon adsorption, ultrafiltration, reverse osmosis and filtration, which only transfer organic compounds from water into another phase, are applied exceptionally in distillation and extraction (Dawood and Sen, 2012; Ngah et al., 2011; Aravind et al., 2016). The chemical methods for the removal of dye, such as oxidation-reduction, complexometric methods, ion exchange and neutralization are in fact the processes with a number of advantages and disadvantages (Nickheslat et al., 2013; Sohrabi and Ghavami, 2008). Among them, a semiconductor is used as a catalyst in the photocatalytic processes. Crystal structures of TiO₂, including rutile and anatase, have been so far tested in many processes. Only the anatase form of TiO, has a high photocatalytic activity, high stability and high value (Fan et al., 2012). In UV/ TiO, system, titanium dioxide absorbs UV light and produces a number of reactive oxygen species (ROS) and hydroxyl radicals (HO[•]) which are very powerful oxidants for degradation of organic pollutants (Zhao et al., 2014). The use of TiO₂ is impaired by its wide band gap (3.2 eV) which activates the photocatalysts that respond only to UV light. UV and visible light account for 4% and 45% of solar energy, respectively (Sun et al., 2012; Zhen Zhu and Wu, 2015). As compared to the wide band gap counterparts, monoclinic BiVO, is an ideal photocatalyst which possesses superior performance due to its narrow band gap (2.4 eV) for water oxidation reactions and activates the photocatalysts that only respond to the visible light (Chatchai et al., 2009; Natarajan et al., 2017). Various studies have been done on the removal of dye by TiO₂ and BiVO₄ nanoparticles. Pereira et al., (2013) found that the UV/TiO₂ photocatalytic system resulted in the removal of high Xanthene dyes. Using the UV/TiO₂ system. Toor et al. (2006) succeeded in removing Direct Yellow 12 dye with 99% removal efficiency in 120 min. Over 40% of 10 mg/L MB dye was degraded by BiVO₄ catalyst (0.08g/100 mL) within 360 min in the presence of visible light. (Li et al., 2016). Hu et al. (2015) also examined the removal of RhB dye by BiVO, under visible light irradiation. They concluded that the tested catalyst could only remove 34% of the dye from the aqueous solution. The design of experimental (DOE) involves a systematic program for performing surveys conducted by the statistical methods. Using this method, controllable input factors can be systematically changed and their effect on output product parameters can be evaluated. Response surface methodology (RSM) is a set of statistical techniques to build models of experimental and applied mathematics. The purpose of this method is to optimize the output variables which are affected by several input variables (Montgomery, 2009). In the above studies, RSM has been used to optimize the process of dye removal by UV/TiO, in a number of cases, including UV/TiO₂ system (Cho and Zoh, 2007; Liu and Chiou, 2005) and UV/TiO₂-coated system (Khataee et al., 2011; Vaez et al., 2012), but the use of BiVO has been very limited. No studies yet have reported on the removal of AO10 dye by RSM using the mentioned nanoparticles. The main objective of this study was to investigate the photocatalytic degradation of an azo dye, called "acid orange 10 (AO10)", in the presence of both TiO₂ particles irradiated by UV-C light and BiVO₄ nanoparticles under visible light of LED lamp (lightemitting diode lamp). Therefore, RSM analysis was used to determine various parameters such as initial dye concentration, initial pH, irradiation time, and catalyst dose. Until 1966, AO10 was used as a drug and cosmetic colorant in the USA, but now its application for the mentioned purposes has been stopped because of its potential hazard to humans. Currently, AO10 is used as a colorant in the textile industries (Bonyadinejad et al., 2016). This study was performed based on the laboratory data in the Faculty of Health, Isfahan University of Medical Sciences in 2018.

MATERIALS AND METHODS

Materials

AO10 dye was purchased from Sigma Aldrich Company and used without further purification. The molecular formula and molecular weight (g/ mol) of AO10 are $C_{16}H_{10}N_2Na_2O_7S_2$ and 452.36, respectively. Fig. 1 displays the structure of this dye. TiO, powder (Merck) was used in the experiments in the anatase form (purity: 99.9 wt%, APS: 20 nm, and SSA: >200 m².g). Bismuth nitrate (Bi(NO₃)₃.5H₂O) and ammonium metavanadate (NH₄VO₃) were also purchased from Merck(Germany) as precursors of BiVO₄. The pH adjustment was done by NaOH and HCl. Distilled water was used to prepare the solution in the whole study.

Synthesis of BiVO

BiVO₄ was prepared using the co-precipitation method. First, 1.17 g NH₄VO₃ and 4.85 g Bi(NO₃)₃.5H₂O were dissolved in 200 mL distilled water. The obtained solution was then mixed at room temperature to reach an orange precipitate. The orange slurry was filtered using filter paper and the residue was washed with distilled water to remove all the ions and salts. The precipitate was dried at 100°C for 5 h. The final product was calcined at 500°C for 4 h and then cooled to the room temperature (Fan *et al.*, 2012). Finally, the prepared BiVO₄ was kept under a desiccator until application.

Photodegradation procedure

The experimental setup of AO10 dye photodegradation by TiO_2 and $BiVO_4$ is illustrated in Fig. 2.



Fig. 1. The studied AO10 chemical structure

TiO, experiments

Photocatalytic oxidation of AO10 was carried out in a 100 mL Pyrex glass vessel containing 0.25 g/100 mL catalyst and 10 mg/L AO10 solution. A 125 W highpressure mercury lamp (Philips) immersed in the inner part of the reactor as a light source. Two mini fans were fixed around the lamps to cool the aqueous solution. Before irradiation, the solution was sonicated for 15 min to disperse TiO₂ uniformity using an ultrasonic (HD 2200 model, Germany Co.). Then, the lamp was turned on to process the required reactions. During irradiation, 4 mL aliquots was withdrawn and then filtered through a 0.22 µm fiberglass filter to remove catalyst particles (Daneshvar *et al.*, 2003; Daneshvar *et al.*, 2004; Pourata *et al.*, 2009).

BiVO₄ experiments

Photocatalytic degradation experiments were done by the degradation of AO10 aqueous solution under visible light irradiation and BiVO, nanoparticles as a photocatalyst. A 12 W LED lamp (white light) located at the top of the reaction vessel was used as a light source. Each experiment was performed at room temperature as follows. 0.25 g of photocatalyst was added into 100 mL of aqueous solution containing 10 mg/L of AO10. Before turning on the LED lamp, it was necessary to sonicate the first mixture for 10 min and later keep it for 1 h in darkness in order to obtain the A010 adsorption/desorption equilibrium by photocatalyst under stirring. At the same irradiation time intervals, a sample (4 mL) was taken from the solution and filtered through a 0.22 µm fiberglass filter to remove the photocatalyst particles (Lili Zhang et al., 2012). The dye decoloration was determined by a spectrophotometer (UV-Vis spectrophotometer,



Magnetic stirrer Fig. 2. Experimental setup of AO10 dye photodegradation

DR-5000, HACH LANGE, USA, $\lambda_{\rm max}$ =475 nm) and a calibration curve (Fig. 3). Eq. 1 was used to calculate the color removal.

Color removal(%) =
$$\frac{ABS_0^{475} - ABS^{475}}{ABS_0^{475}} \times 100$$
 (1)

Where, ABS_0^{475} and ABS_0^{475} are absorbances at 475 nm before and after treatment, respectively.

Experimental design

Response surface methodology (RSM) is commonly used in the optimization of chemical reactions and/ or industrial experimentations to explore nonlinear relationships between continuous predictor variables and the dependent variables. RSM allows for the quadratic surfaces to fit the observed dependent variable values and to determine the predicted maximum (or minimum) values for the dependent variables of interest. In the present study, the rotatable experimental plan was used as a Central Composite Design (CCD) for the optimization of UV/TiO₂ and UV–Vis/BiVO₄ treatment of AO10 dye. The effects of four main factors (initial dye concentration, initial pH, irradiation time, and catalyst dosage) on UV/TiO₂ and UV–Vis/BiVO₄ processes were investigated. Experimental ranges and levels of



Table 1: Experimental ranges and levels of independent variables for UV/TiO, process of AO10 removal

	Ranges and levels				
Independent variables	-2	-1	0	+1	+2
Initial dye concentration (mg/L) (A)	10	20	30	40	50
Initial pH (B)	1	4	7	10	13
Irradiation time (min) (C)	0	5	10	15	20
Catalyst dosage (g/100 mL) (D)	0.05	0.1	0.15	0.2	0.25

Table 2: Experimental range and levels of independent variables for UV-Vis/ BiVO, process of AO10 removal

	Ranges and levels					
Independent variables	-2	-1	0	+1	+2	
Initial dye concentration (mg/L) (A)	10	20	30	40	50	
Initial pH (B)	3	4.5	6	7.5	9	
Irradiation time (min) (C)	0	90	180	270	360	
Catalyst dosage (g/100 mL) (D)	0.05	0.1	0.15	0.2	0.25	

independent variables for the studied AO10 removal processes are given in Tables 1 and 2, respectively. For statistical calculations, the value of independent variables X_i (the real value of an independent variable) was coded as x_i (dimensionless coded value of an independent variable) according to Eq. 2.

$$x_i = \frac{X_i - X_0}{\Delta X_i}, i = 1, 2, 3, ..., n$$
 (2)

Where, x_0 is the value of x_i at the center point, and Δx_i represents the step change.

The data obtained from the experimental runs were analyzed by Design-Expert 10.0.1 software. These data can be presented in graphical forms, or in 3-D response surface and 2-D contour plots. The regression equation related to the quadratic response surface regression design for predicting the optimal conditions is presented by Eq. 3.

$$Y = \beta_0 + \sum_{i=1}^{n} \beta_i x_i + \sum_{i=1}^{n} \beta_{ii} x_i^2 + \sum_{i=1}^{n-1} \sum_{i=j+1}^{n} \beta_{ij} x_i x_j$$
(3)

Where, Y is defined as the response factor for the decolorization efficiency, β_o is the constant coefficient, β_i , β_{ij} , β_{ij} are the regression coefficients for the linear parameters, quadratic and interaction effect, respectively, and x_i and x_j are the design variables. Furthermore, a successful application of RSM to design optimization of experiment projects can lead to reducing the high cost of analysis methods and their associated numerical noise (Yingling *et al.*, 2011).

RESULTS AND DISCUSSION

Analysis of nanoparticles

The X-ray diffraction (XRD, D8ADVANCE model, Bruker Company, Germany) patterns of nano-TiO₂ in anatase phase and the prepared BiVO₄ nanoparticles were obtained by Cu K α radiation (Figs. 4a and 4b). Field-emission scanning electron microscope (FE-SEM, MIRA3 model, TESCAN Co.) analysis was used to study the shape and uniformity of the nano-TiO₂ and BiVO₄ powder samples (Figs. 4c and 4d). It should be noted that the XRD data were collected for both TiO₂ and BiVO₄ nanoparticles at diffraction angles of 20° to 80° and 5° to 90°, respectively. There is a strong and sharp diffraction peak at 25.35° in the anatase phase and at 29° for BiVO₄ nanoparticles, which can prove that the two nanoparticles conform to the standard samples JCPDS PDF No. 14-0688 and JCPDS PDF No. 21-1272, respectively. TiO₂ nanoparticles are in spherical form and have a size of about 20 nm. However, according to Fig. 4d, the BiVO, nano-catalyst is completely spherical and uniform and has a size of about 30 nm. FT-IR (Tensor 27-Equinox 55 model, Bruker) has been used to identify functional groups in the catalysts structure in the wavelength range of 400-4000/cm. Based on Fig. 5, TiO₂ and BiVO₄ samples have been used for the FT-IR spectrum to study the functional groups. Figs. 5a and 5b shows the spectra related to titanium dioxide and bismuth vanadate in both catalysts with a broad-spectrum in the range of 3400/cm referring to OH groups. Also, in the range of 1630/cm, the presence of bending vibrations of the H₂O molecule adsorbed on the catalyst surface is clearly shown (Venkatachalam et al., 2007). In Fig. 5a, the appearing peak at 600-1000/cm represents the Ti-O vibration (Jian Zhu et al., 2007). In Fig. 5b, the VO³⁻ symmetry bending is related to the absorption band at 480/cm. Also, the V-O-V band in the range of 726/cm indicates the stretching vibration (Dong et al., 2014; A Zhang and Zhang, 2009). Fig. 6 confirms the photocatalytic properties of TiO, and BiVO, nanoparticles, which removed the dye from the aqueous solution by UV/ TiO, more clearly.

The results of central composite design experiments

The experiments of combined effects of parameters were performed in different conditions using the design of experiments. Experimental plan and results showing the coded values of the variables along with their actual and predicted values are given in Table 3. The regression analyses of AO10 dye removal in terms of coded units are presented in Tables 4 and 5 for UV/ TiO₂ and UV–Vis/BiVO₄, respectively. The final equation in terms of coded factors for TiO₂ can be written Eq. 4.

Y = +69.22 - 11.69 * A - 1.13 * B + 18.74 * C + 3.32 * D + 0.69* AB + 0.74 * AC + 0.35 * AD + 0.40 * BC - 0.23 * BD - 0.39 * CD + 1.19 * A² + 2.63 * B² - 7.36 * C² - 0.21 * D² (4)

The final equation in terms coded factors for ${\rm BiVO}_4$ can be expressed by Eq. 5.

Y=+25.27292 - 1.07421 * A - 3.30944 * B +0.065926 * C +92.59167 * D + 0.069000 * AB - 3.48611 * AC - 2.28250 * AD - 1.38889 * BC + 4.53333 * BD + 0.11694 * CD + 0.012567 * A² - 0.017037 * B² - 1.13837 * C² - 88.33333 * D² (5)

Tables 4 and 5 indicate that the coefficients for initial dye concentration (A) (P<0.0001), irradiation time (C) (P<0.0001), and catalyst dose (D) (P=0.0043), except for initial pH (B) (P=0.2691) for TiO₂, are highly significant. However, for BiVO₄ all variables are significant. In the quadratic form, B² (P=0.0121) and C² (P=< 0.0001) for TiO₂ were significant, and A² (P<0.0001) and C² (P=0.0005) for BiVO₄ were highly significant. The interaction terms were not significant for TiO₂ and only AB (P=0.0016), and AD (P=0.0007) were highly significant for BiVO₄. ANOVA showed that for TiO₂ and BiVO₄, the *P*-values for all models were

close to 0, implying that the quadratic models were significant. The values of $R^2_{(adj)}$ for TiO₂ and BiVO₄ were 95.26% and 94.91%., respectively, indicating the high accuracy of the model.

Role of TiO, in A010 degradation

Fig. 7 shows the effect of UV alone, TiO_2 alone and UV/TiO₂ on contact time in the AO10 dye removal. As can be seen, after 8 min of UV irradiation in the presence of TiO_2 , 100% of the dye was degraded. This efficiency decreases to about 84% in the absence of TiO₂ for UV irradiation (photolysis). Fig. 7 also shows



Fig. 4: Characteristics of nano-photocatalysts: a) XRD pattern of nano- TiO_2 in the anatase form; b) XRD pattern of the prepared $BiVO_{4;}$ c) FE-SEM of nano-TiO₃; and d) FE-SEM of the prepared $BiVO_4$

no change in dye concentration when the UV lamp is turned off and TiO, particles are used in darkness. In this regards, AO10 was more effectively degraded in the UV/TiO, system as compared to the time that either UV or TiO, was used alone. The first step in photodegradation by the UV/TiO, system is to generate electrons and holes within titanium dioxide particles (Eq. 6). Hydroxyl radicals (OH) are generated at the surface by valence band (h_{VB}^+) , and the conduction band electrons $(\bar{e_{CB}})$ reduce the amount of oxygen adsorbed onto the surface. Moreover, the generated hydroxyl radicals to attack the organic pollutants are present at or near the surface of TiO₂. They induce the photocatalytic removal of the dye according to Eqs. 7 to 12 (Fujishima et al., 2000; Hoffmann et al., 1995; Jiang and Zhang, 2010; Tang and An, 1995).

$$TiO_2 + hv \rightarrow TiO_2 (e_{CB}^- + h_{VB}^+)$$
(6)

$$h_{VB}^{+} + H_2 O_{(ads)} \rightarrow H^+ + OH_{(ads)}^*$$
(7)

$$h_{VB}^{+} + OH_{(ads)}^{-} \rightarrow OH_{(ads)}^{*}$$
(8)

$$e_{CB}^{-} + O_{2 (ads)} \rightarrow O_{2 (ads)}^{-}$$
(9)

$$OH^*_{(ads)}$$
+ dye \rightarrow degradation of the dye (10)

$$h_{VB}^+ + dye \rightarrow oxidation of dye$$
 (11)

$$e_{CB}^{-}$$
 +dye \rightarrow reduction of dye (12)

Also, the reactions made by the BiVO₄ catalyst in aqueous solution can be similar to those made by



Fig. 5: FTIR (Fourier Transform Infrared Spectroscopy) spectra of: a) TiO₂, and b) BiVO₄

 $TiO_{2^{\prime}}$ except that $BiVO_4$ is activated by visible light with no charge recombination (Fig. 8).

Comparison of AO10 removal at different initial concentrations

According to Fig. 9, the AO10 photodegradation decreases with the increase of its initial concentration. It seems that the main reason for the increase of initial concentration in dye is that its molecules are adsorbed more and more onto the surface of photocatalyst. High amount of dye concentration leads to reduction in generation of OH^{*} radicals on the surface of catalyst. In this condition, the terms of inhibitory effects on the reaction of dye molecules along with photogenerated holes or hydroxyl radicals



Fig. 6. The photographic representation of dye removal a) before, b) after using UV/TiO2, and c) after using UV–vis/BiVO4

may occur due to the fact that the active sites are covered by dye ions. Another reason that can be effective in removal efficiency at high concentrations of dye is the effect of UV screening. In this condition, a significant amount of UV may be absorbed by the dye molecules rather than the catalyst and the photons never reach the photocatalyst surface, leading to decrease of photocatalytic removal efficiency (Asiltürk *et al.*, 2006; Konstantinou and Albanis, 2004; Nikazara *et al.*, 2007; Pourata *et al.*, 2009).

Interactions of the studied variables in dye removal

Fig. 10a shows the percent of degradation efficiency for an irradiation time of 8 min and TiO, dosage of 0.25 g/100 mL obtained as a function of initial pH and initial dye concentration. The pH effect on the photocatalytic degradation of AO10 was investigated in the pH range of 1 to 13. An increase in AO10 dye degradation with the decrease of pH to below 7 can be explained by the UV/TiO₂ system in acidic solutions. A study by Shu and Chang (2005) showed the increase of efficiency by the decrease of pH to below 7. Hence, in acidic pH range, the dye will be predominantly in its protonated form, and its strong adsorption onto the TiO, surface and the corresponding high rate of degradation will occur. At these conditions, the surface will be positively charged and the TiO, surface can effectively adsorb the negatively charged dye anion (Gupta et al., 2012; Sakthivel et al., 2002; Gupta et al., 2016). At pH values of above 7, surface will negativity inhibit photocatalytic rates and lead



Fig. 7: Effect of TiO₂ on AO10 removal at different conditions as a function of irradiation time; [TiO₂] = 0.25 g/100 mL, dye concentration=10 mg/L, pH=3.5

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					Removal efficiency (%)			
Run	А	В	С	D	Ti	O ₂	Bi\	/04
order					Exp.	Pred.	Exp.	Pred.
1	0	0	0	2	77.88	75.02	9.97	9.97
2	2	0	0	0	99.76	97.36	9.97	9.97
3	-1	-1	-1	1	68.82	64.98	15.79	15.65
4	-1	1	1	-1	87.17	91.39	7.35	8.56
5	1	-1	1	-1	69.76	69.79	8.02	8.09
6	1	-1	-1	1	40.25	39.42	7.01	4.50
7	1	-1	-1	-1	33.55	30.86	6.21	5.13
8	-1	-1	-1	-1	58.23	57.82	10.94	10.51
9	0	0	0	0	69.22	69.22	9.97	9.97
10	-1	1	-1	-1	52.82	53.81	5.41	5.10
11	-1	-1	1	1	98.00	99.40	21.82	21.97
12	0	0	0	-2	63.94	61.75	4.44	4.50
13	0	0	0	0	69.22	69.22	9.97	9.97
14	0	0	0	0	69.22	69.22	9.97	9.97
15	1	1	1	-1	64.69	70.18	6.51	6.06
16	1	1	1	1	72.48	76.29	9.77	10.10
17	-1	-1	1	-1	94.00	93.78	14.29	14.73
18	1	-1	1	1	76.16	76.81	11.04	10.76
19	0	0	0	0	69.22	69.22	9.97	9.97
20	0	0	-2	0	0.000	2.30	0.000	2.02
21	-1	1	-1	1	56.70	60.06	11.76	11.59
22	0	-2	0	0	76.56	82.03	11.91	12.86
23	-1	1	1	1	91.76	96.10	5.41	5.10
24	0	2	0	0	88.00	77.49	7.03	6.78
25	0	0	2	0	84.61	77.27	11.87	10.55
26	0	0	0	0	69.22	69.22	9.97	9.97
27	0	0	0	0	69.22	69.22	9.97	9.97
28	2	0	0	0	53.23	50.59	7.11	8.77
29	1	1	-1	-1	27.64	29.63	4.10	3.85
30	1	1	-1	1	35.42	37.28	6.81	5.78

Table 3: Experimental plan and results of the central composite design

Table 4: Estimated regression coefficients for UV/TiO₂ process of AO10 removal

Factor	Coefficient	SE coefficient	t	Р
Intercept	69.22	1.98	34.959	< 0.0001
А	-11.69	0.99	-11.808	< 0.0001
В	-1.13	0.99	-1.141	0.2691
С	18.74	0.99	18.929	< 0.0001
D	3.32	0.99	3.353	0.0043
AB	0.69	1.21	0.570	0.5746
AC	0.74	1.21	0.611	0.5490
AD	0.35	1.21	0.289	0.7760
BC	0.40	1.21	0.330	0.7436
BD	-0.23	1.21	-0.190	0.8530
CD	-0.39	1.21	-0.322	0.7544
A ²	1.19	0.92	1.293	0.2180
B ²	2.63	0.92	2.858	0.0121
C ²	-7.36	0.92	-8	< 0.0001
D ²	-0.21	0.92	-0.228	0.8251

to the decrease of the removal efficiency. Park *et al.* (2003) obtained the same result, in which the removal efficiency of dye decreased with the increase of pH to over 7. Some stuidies have shown that increase

of pH to over 10 in solution favors OH* formation on the catalyst surfaces and is directly responsible for initiating the dye oxidation (Lung-Chyuan and Tse-Chuan, 1993; Poulios and Aetopoulou, 1999). Dye removal generally exhibits maximum decolorization at highly acidic or alkaline pH conditions. Fig. 10b displays the percent of degradation efficiencies for pH of 3.5 and TiO, dosage of 0.25 g/100 mL, obtained as a function of irradiation time and initial dye concentration. Equilibrium time can be considered as one of the most important design parameters in the photocatalytic process when a catalyst is used in the removal of organic pollutants. The plots illustrate that UV/TiO, has a high efficiency at all experimental intervals. The results revealed that 100% of AO10 dye was removed in 8 min. Fig. 10c illustrates the percent of removal efficiencies for an irradiation time of 8 min and pH of 3.5, obtained as a function of TiO, (g/100 mL) and initial dye concentration. The amount of catalyst loading is an important factor for detecting the adsorption capacity of solid for the removal of organic pollutants. Nanoparticle concentration has a great influence on the amount of decomposition in the presence of UV light, so that the removal efficiency increases in the range of 0.05 to 0.25 g/100 mL at a fixed amount of dye and contact time of 8 min. Abou-Gamra and Ahmed (2015) and Garcia and Takashima (2003) obtained similar results and concluded that the UV/TiO, process increased the removal efficiency of dye by increasing the catalyst dose.

Role of BiVO₄ in A010 degradation

Fig. 11 shows that with the increase of AO10 concentration, its decomposition decreases by irradiation time. However, the removal efficiency of this process was much lower than that of the UV/TiO,

Table 5: Estimated regression coefficients for UV–Vis/BiVO $_4$ process of AO10 removal				
Factor	Coefficient	SE coefficient	t	Р
Intercept	25.27	7.74	3.264	< 0.0001
A	-1.07	0.19	-5.631	< 0.0001
В	-3.31	1.40	-2.364	0.0316
С	0.066	0.020	3.3	0.0048
D	92.59	38.49	3.353	0.0295
AB	0.069	0.018	2.405	0.0016
AC	-3.486	3.004	-1.160	0.2640
AD	-2.28	0.54	-4.222	0.0007
BC	-1.389	2.003	-0.693	0.4985
BD	4.53	3.60	1.258	0.2277
CD	0.12	0.060	0.2	0.0706
A ²	0.013	2.065	0.006	< 0.0001
B ²	-0.017	0.092	-0.184	0.8552
C ²	-1.138	2.549	-0.446	0.0005
D ²	-88.33	82.59	-1.069	0.3017









Fig. 9: Effect of initial concentration of AO10 on photo-oxidative removal of dye; [TiO,] = 0.25 g/100 mL, pH=3.5

Catalyst Lig	ght source	Dye concentration (mg/L)	Catalyst dosage (g/100 mL)	Time (min)	Efficiency (%)	References
ZnO	Solar	10	0.4	30	76.92	(Velmurugan and Swaminathan, 2011)
TiO ₂	UV	30	0.1	120	99	(Toor <i>et al.,</i> 2006)
TiO ₂	UV	50	0.6	240	93	(Ong et al., 2012)
Ag ₃ VO ₄	Visible	10	0.05	60	51	(Xu <i>et al.,</i> 2010)
BiVO ₄	Visible	10	0.08	360	46	(Li <i>et al.,</i> 2016)
BiVO ₄	Visible	10	0.06	180	30	(Shi <i>et al.,</i> 2018)
PbWO4	UV	20	0.05	300	100	(Yu <i>et al.,</i> 2013)
TiO ₂	UV	11.88	0.17	12.87	100	The present study
BiVO ₄	Visible	10.91	0.23	320.26	36.93	The present study

Table 6: Comparison of the two systems studied in this work with other processes

Table 7: Optimum values for degradation of AO10 dye by UV/TiO, and UV–Vis/BiVO, processes

Factors	Linite	Optimum values		
Factors	Units	UV/TiO ₂	UV–Vis/BiVO4	
Initial dye concentration	mg/L	11.88	10.91	
Initial pH	-	4.59	3.23	
Irradiation time	min	12.87	320.26	
Catalyst dose	g/100 mL	0.17	0.23	
Predicted degradation efficiency	(%)	100	36.93	
Observed degradation efficiency	(%)	100	34.60	

showed in Fig. 9. The photocatalytic capability of the synthesized catalyst $BiVO_4$ semiconductor was also investigated by the removal of AO10 under various conditions including pH values, dosage of catalyst, irradiation time and initial dye concentration. As shown in Fig. 12a, the pH range of 3 to 9 was investigated

and higher dye removals were obtained at low initial pH values, especially pH 3. On the other hand, AO10 removal percent decreased with the increase of pH value and decolorization efficiency reached 26.7% at pH 9, irradiation time of 360 m, and catalyst dose of 0.25 g/100 mL. This can be attributed to the change

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(c)

Fig. 10: The 3-D response surface and 2-D contour plot of dye removal efficiency (%) as a function of initial dye concentration (mg/L) in terms of a) initial pH b), irradiation time (min), and c) TiO₂ dosage (g/100 mL)



Fig. 11: Effect of initial concentration of AO10 on photo-oxidative removal of dye; [BiVO,] = 0.25 g/100 mL, pH=3

in the surface charge of the adsorbent which can have a positive or negative charge at different pH values. However, experiments showed that the initial pH had no significant effect on AO10 dye removal. Fig. 12b shows the decrease of removal efficiency as only 39% of total AO10 was removed within 360 min. The increase of AO10 removal with the increase of time indicates the dye adsorption by the catalyst at higher contact times. The results presented in Fig. 12c indicate that decolorization efficiency increased with the increase of adsorbent dosage from 0.05 to 0.25 g/100 mL at pH 3. It is obvious that when the initial concentration of catalyst was increased, the reaction resulted in the highest removal efficiency. This could be attributed to the availability of larger surface area and more adsorption sites at higher adsorbent doses. Furthermore, the maximum dye removal efficiency occurred at the maximum catalyst dosage (0.25 g/100 mL), and decolorization efficiency decreased with the increase of the initial dye concentration. At the high dye concentration, the available active sites on the surface of catalyst are limited, leading to reduction of removal percentage in dye ions. Therefore, it can be concluded that the BiVO, semiconductor prepared by co-precipitation method has a little efficiency in AO10 degradation at all experimental intervals.

Comparison between the present study and previous studies

Table 6 compares the photocatalytic activity of the systems studied in this paper with other processes for

the removal of dye reported in previous studies. As shown in Table 6, the rate of dye removal in the UV light with TiO₂ nanoparticle under optimum condition was remarkably higher than that of dye removal in other systems for degradation of dye. However, the rate of dye removal in UV–Vis/BiVO, process was low. Ong et al. (2012) observed 93% of 50 mg/L dye degradation during 240 min irradiation time in a UV light with 0.6 g/100 mL TiO₂. Around 76% of 10 mg/L dye was degraded in the photocatalytic process using ZnO catalyst under solar light within 30 min (Velmurugan and Swaminathan, 2011). The rate of 10mg/L dye degradation in a UV–Vis/Ag₂VO₄ process was observed to be 51% (Xu et al., 2010). This can be due to the fact that the TiO, nanoparticle is more efficient than other methods for enhancing photocatalytic activity for removing dye in the presence of UV light.

Determination of optimum conditions for TiO_2 and $BiVO_4$

Selection of the desired goal for each factor in terms of degradation efficiency was done based on "maximization" to obtain the maximum dye removal. Optimized values of the experimental design for TiO_2 and $BiVO_4$ are shown in Table 7. The actual values were in good agreement with the results achieved through RSM. In this way, the findings from optimization of the response surface were validated. According to the results obtained by the RSM model prediction and the experimental data validation, it can be concluded that the maximum degradation of AO10 is achieved using RSM.

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Fig. 12: The 3-D response surface and 2-D contour plot of the dye removal efficiency (%) as a function of initial dye concentration (mg/L) in terms of a) initial pH; b) irradiation time (min), and c) BiVO₄ dosage (g/100 mL)

CONCLUSION

The photocatalytic oxidation of AO10 was investigated by TiO, catalyst suspension and irradiation with a UV-C lamp (125 W) and BiVO₄ nanoparticles under visible light of an LED lamp (12 W). In the optimum conditions of process factors, the removal efficiencies of 100% and 36.93% were obtained for UV/TiO, and UV-Vis/BiVO₄ processes, respectively. According to the results, the degradation efficiency by TiO₂ as high as to remove all the dye in the solution, but the dye degradation efficiency using the synthesized BiVO, by co-precipitation method was low and incomplete. Therefore, it seems necessary to use the BiVO4 /TiO2 composite process to remove AO10 dye in further studies. The results obtained in this study showed that pH had not much effect on the AO10 removal process, and the dye can easily be removed at different pH values for both nanoparticles, especially TiO₂. Considering the limitations of traditional systems, application of RSM in optimization of design can effectively reduce the cost of expensive analytical methods and the related numerical disturbances. In the present study, it was indicated that RSM was an ideal method to optimize the independent variables and maximize the removal of dye.

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CONFLICT OF INTERESTS

The author declares that there is no conflict of interests regarding the publication of this manuscript. In addition, the ethical issues, including plagiarism, informed consent, misconduct, data fabrication and/ or falsification, double publication and/or submission, and redundancy have been completely observed by the authors.

ABBREVIATIONS

2-D	2-dimentional
3-D	3-dimentional
Α	Initial dye concentration (mg/L)

ABS_{0}^{475}	Absorbance at 475 nm before treatment		
ABS ⁴⁷⁵	Absorbance at 475 nm after treatment		
Ag ₃ VO ₄	Silver vanadate(V)		
AO10	Acid Orang10		
В	рН		
BiVO ₄	Bismuth vanadate		
С	Irradiation time (min)		
СВ	Conduction band		
CCD	Central Composite Design		
ст	Centimeter		
Co.	Company		
CO ₂	Dioxide carbon		
D	Catalyst dosage (g/100 mL)		
DOE	Design of experimental		
e_{CB}^-	Excited electron		
Exp.	Experimental value		
	Field-emission scanning electron		
FE-JEIVI	microscope		
Fig.	Figure		
FTIR	Fourier Transform Infrared Spectroscopy		
g	Gram		
h⁺	hole		
НО	Hydroxide		
H ₂ O	Water molecule		
min	Minute		
mL	Milliliter		
mg/L	Milligram per liter		
<i>O</i> ₂	Oxygen molecule		
•O ⁻ 2	Oxygen radical		
OH*	Hydroxide radical		
Ρ	P value		
PbWO ₄	Lead tungstate		
Pred.	Predicted value		
RhB	Rhodamine B		
ROS	Reactive Oxygen Species		
RSM	Response surface methodology		
SE	Standard error		
t			
	l value		

UV	Ultra violet
VB	Valence band
Vis	Visible
<i>x</i> ₀	The value of the $\mathbf{x}_{_{\mathrm{i}}}$ at the center point
x _i	Dimensionless coded value of an independent variable
XRD	X-ray diffraction
ZnO	Zinc oxide
Δx_{i}	Step change
β_o	Constant coefficient
β_i	Linear effect
β_{ii}	Quadratic effect
β_{ij}	Interaction effect
°C	Celsius degrees
$\lambda_{_{max}}$	Maximum wavelength
Y	Decolorization efficiency (%)
%	Percentage
μm	Micrometer

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